AMENDMENTS TO THE CLAIMS

- 1. (Currently Amended) An ion exchange membrane comprising:
- (A) a porous film layer having pores with an average pore diameter of 0.01 to 2 μ m; and
 - (B) a surface layer existent on at least one side of the porous film,

wherein the pores of the porous film layer (A) are filled with a crosslinked ion exchange resin and the surface layer comprises (a) an inorganic filler having an average primary particle longest diameter which is 0.1 times or more the average pore diameter of the pores of the porous film layer and 50 μ m or less and (b) a crosslinked ion exchange resin, wherein each of the crosslinked ion exchange resins is produced from at least one crosslinkable monomer selected from the group consisting of crosslinked with a polyfunctional vinyl [[compound]] monomer and [[or]] a polyfunctional methacrylic acid derivative monomer, and wherein the inorganic [[particle]] filler is a lamellar particle.

2. (Cancelled)

- 3. (Withdrawn) A process for producing the ion exchange membrane of claim 1, comprising the steps of:
- (1) contacting a porous film having pores with an average pore diameter of 0.01 to 2 μ m to a suspension containing an inorganic filler having an average primary particle longest diameter which is 0.1 time or more the average pore diameter of the pores of the porous film and 50 μ m or less and a polymerizable monomer selected from the group consisting of a

polymerizable monomer which provides an ion exchange resin when it is polymerized and a

polymerizable monomer which provides an ion exchange resin precursor when it is polymerized

in order to infiltrate the suspension into the pores of the porous film and to adhere the suspension

to the surface of the porous film;

(2) polymerizing the polymerizable monomer contained in the suspension in the

pores and on the surface of the porous film; and

(3) converting the ion exchange resin precursor into an ion exchange resin when the

ion exchange resin precursor is obtained by polymerization in the step (2).

4. (Withdrawn) A process for producing the ion exchange membrane of claim 1,

comprising the steps of:

(1) contacting a porous film having pores with an average pore diameter of 0.01 to 2

μm to a suspension containing an inorganic filler having an average primary particle longest

diameter which is 0.1 time or more the average pore diameter of the pores of the porous film and

50 µm or less, a resin selected from the group consisting of an ion exchange resin and an ion

exchange resin precursor, and a solvent in order to infiltrate the suspension into the pores of the

porous film and to adhere the suspension to the surface of the porous film;

(2) removing the solvent contained in the suspension in the pores and on the surface

of the porous film; and

(3) converting the ion exchange resin precursor into an ion exchange resin when the

suspension in the step (2) contains the ion exchange resin precursor.

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- 5. (Original) A diaphragm for a direct methanol type fuel cell which comprises the ion exchange membrane of claim 1.
- 6. (Original) A direct methanol type fuel cell comprising the diaphragm for a direct methanol type fuel cell of claim 5.
- 7. (Previously Presented) The ion exchange membrane of claim 1, wherein the porces in the porcus film layer have an average pore diameter of 0.01 to 1 μ m.
- 8. (Previously Presented) The ion exchange membrane of claim 1, wherein the porous film layer (A) has a void volume of 20 to 95%.
- 9. (Previously Presented) The ion exchange membrane of claim 8, wherein the void volume of the porous film layer (A) is 30 to 90%.
- 10. (Previously Presented) The ion exchange membrane of claim 1, wherein the porous film layer (A) has a gas permeability of 1,000 sec or less.
- 11. (Previously Presented) The ion exchange membrane of claim 10, wherein the porous film layer (A) has a gas permeability of 500 sec or less.

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- 12. (Previously Presented) The ion exchange membrane of claim 1, wherein the porous film layer (A) has a thickness of 5 to 150 μ m.
- 13. (Previously Presented) The ion exchange membrane of claim 1, wherein the inorganic filler has an average primary particle longest diameter which is 0.2 times or more the average pore diameter of the pores of the porous film layer and $10 \mu m$ or less.
- 14. (Previously Presented) The ion exchange membrane of claim 1, wherein the aspect ratio of the lamellar particle is 200 to 1,000.
- 15. (Previously Presented) The ion exchange membrane of claim 1, wherein the lamellar particle is at least one selected from the group consisting of montmorillonite, bentonite, smectite, hectorite, beidellite, sauconite, perovskite, saponite, kaolin, sericite, mica, talc and lamellar silicate.
- 16. (Previously Presented) The ion exchange membrane of claim 1, wherein the inorganic filler is treated with a silane coupling agent or a surface active agent.
- 17. (Previously Presented) The ion exchange membrane of claim 1, wherein the ion exchange resin contained in the surface layer and the ion exchange resin in the pores form a continuous phase without an interface.

- 18. (Previously Presented) The ion exchange membrane of claim 1, wherein the ion exchange resin in the pores of the porous film layer (A) further comprises an inorganic filler.
- 19. (Previously Presented) The ion exchange membrane of claim 18, wherein the concentration of inorganic filler in the pores is lower than the concentration of inorganic filler in the surface layer.
- 20. (Previously Presented) The ion exchange membrane of claim 19, wherein the ion exchange resin contained in the surface layer and the ion exchange resin in the pores form a continuous phase without an interface.